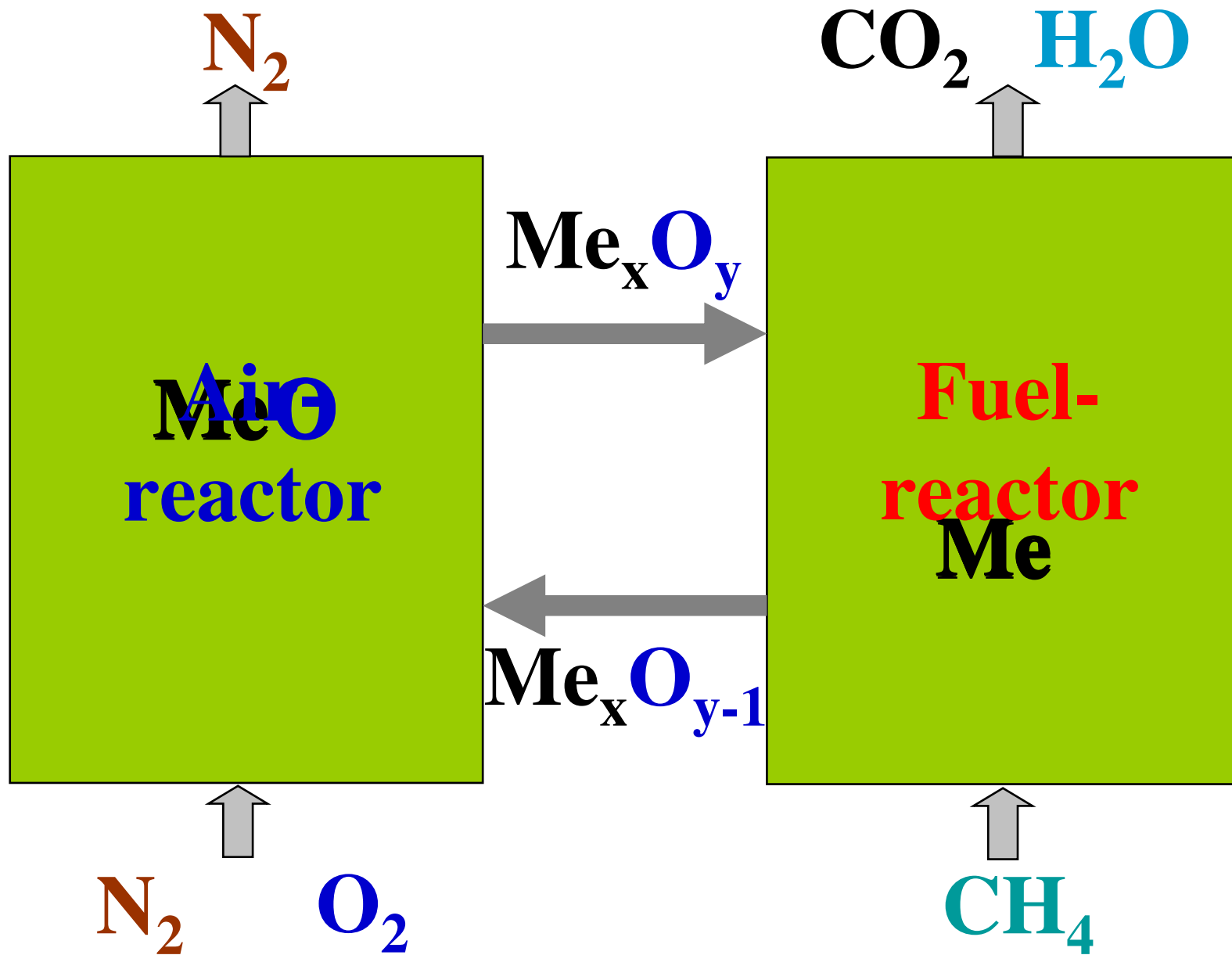


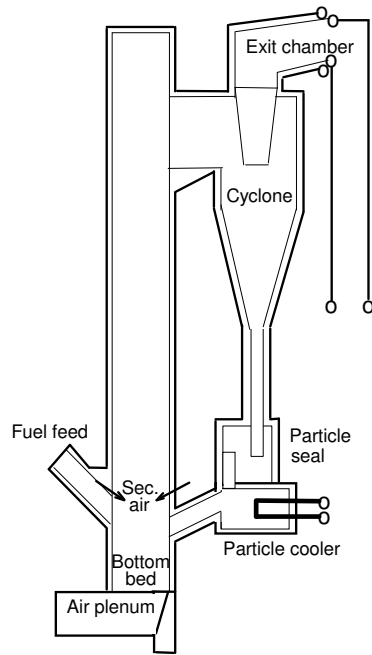
**HYDROGEN AND POWER PRODUCTION  
WITH INTEGRATED  
CARBON DIOXIDE CAPTURE  
BY  
CHEMICAL-LOOPING REFORMING**

**Magnus Rydén  
Anders Lyngfelt  
Chalmers University of Technology**

**Vancouver, September 2004**

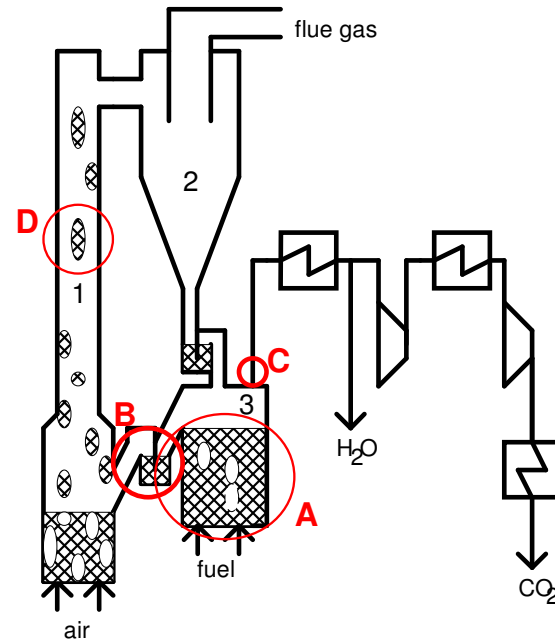


## circulating fluidized-bed combustion of solid fuels



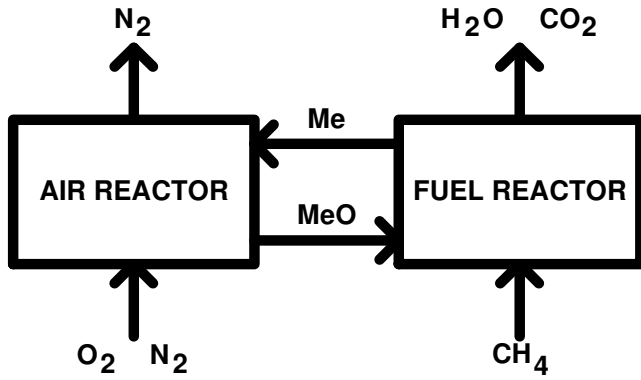
**commercial:**  
**250 MWe in operation**  
**600 MWe designed**

## chemical-looping combustion



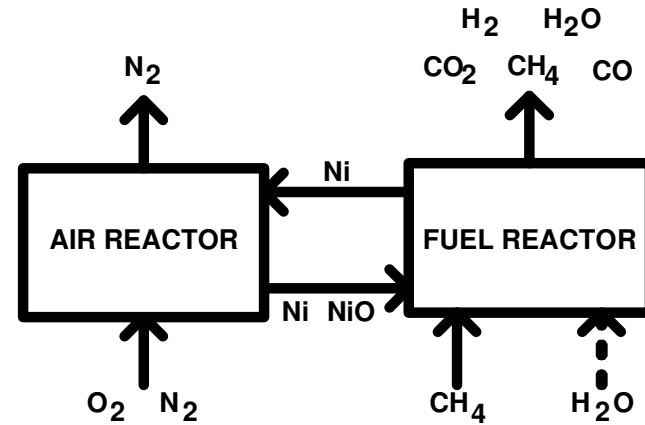
- A** extra fluidized-bed
- B** extra particle lock
- C** additional gas outlet
- D** no gas residence time criteria

chemical-looping combustion



full fuel conversion

chemical-looping reforming



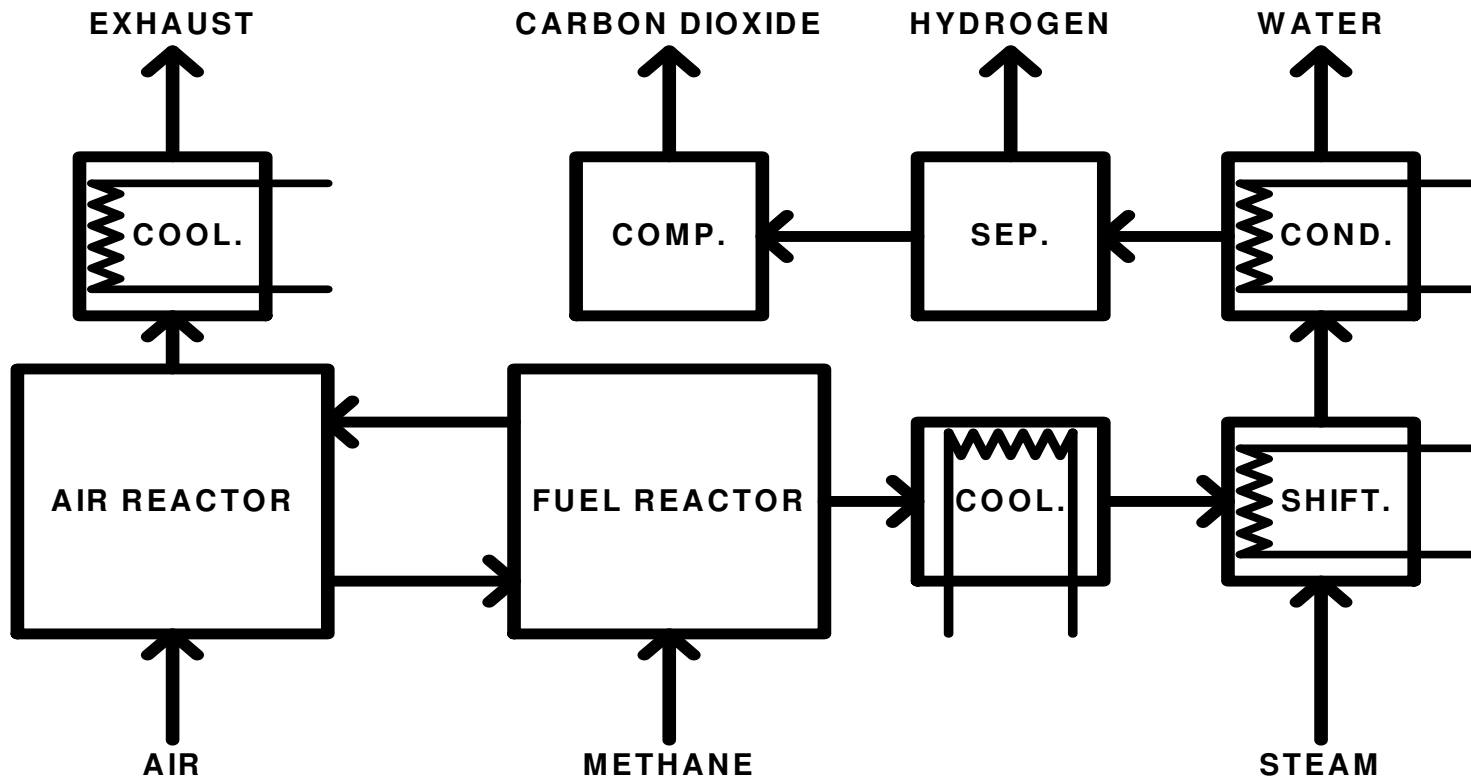
partial fuel conversion

3 × added fuel  
(~1/3 cost/MW fuel)

chemical-looping reforming  
suitable for scaling-up  
undiluted  $\text{CO}_2/\text{H}_2$

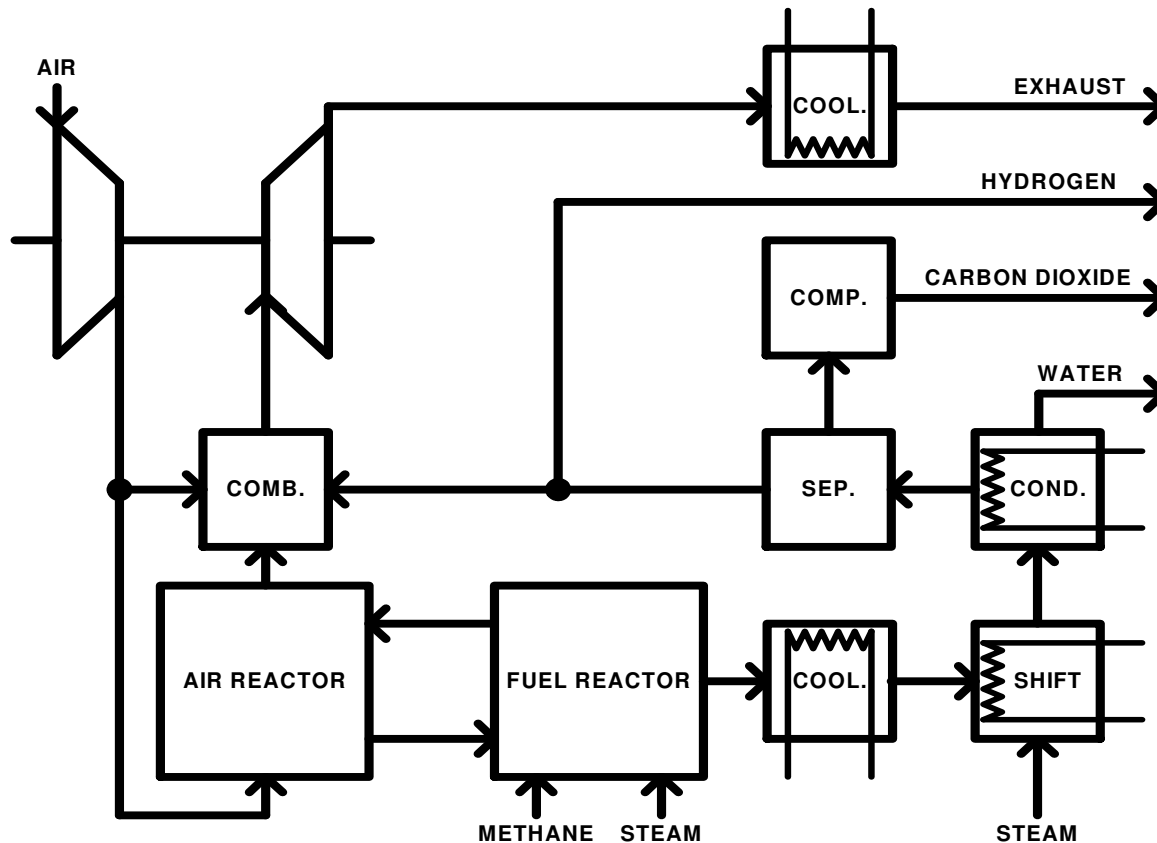
conventional reforming  
in use

# ATMOSPHERIC CLR



Simplified process scheme for case 1A, atmospheric CLR by partial oxidation. Preheating of fuel, air and steam is not shown.

# PRESSURIZED CLR



Simplified process scheme for case 2B, pressurized CLR with internal H<sub>2</sub> combustor.  
Integration with steam cycle and preheating of fuel and steam is not shown.

## chemical-looping reformation cases

### atmospheric

1A partial oxidation

1B autothermal, (partial oxidation and some steam added)

1C autothermal, heat used in steam cycle

### pressurized+combined cycle

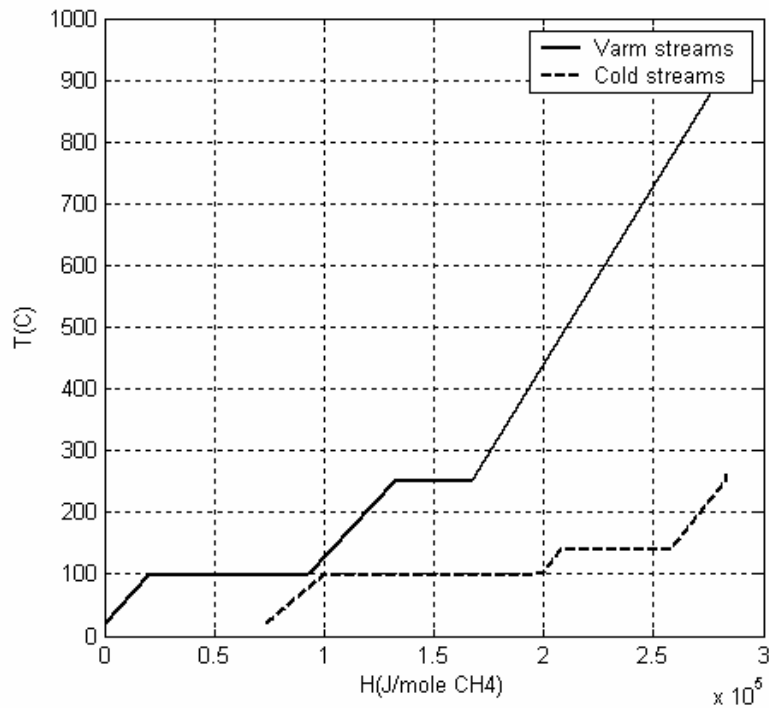
2A autothermal, turbine inlet 1017 C

2B autothermal, H<sub>2</sub> used for temperature increase

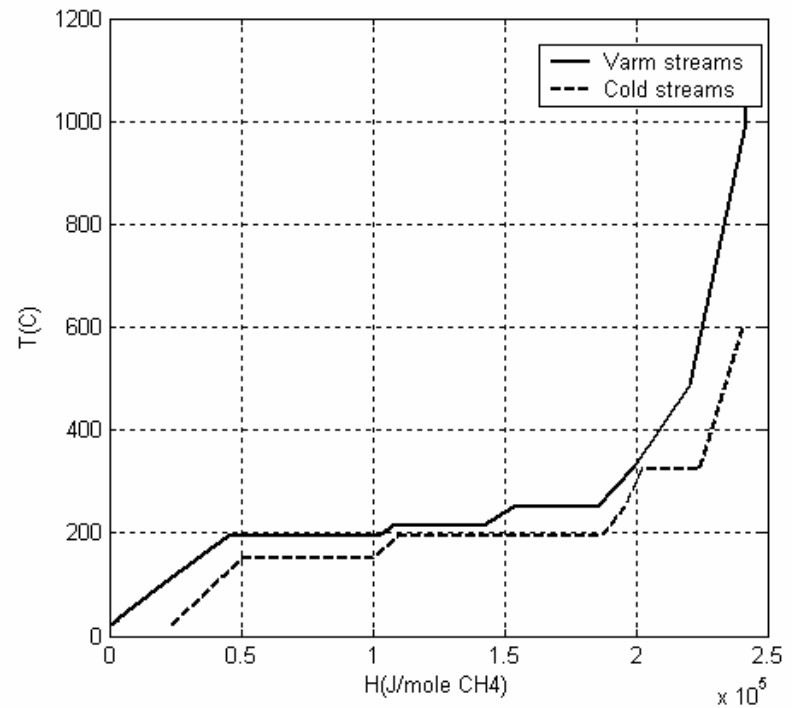
2C autothermal, high temperature air reactor 1172 C



# THERMAL PERFORMANCE

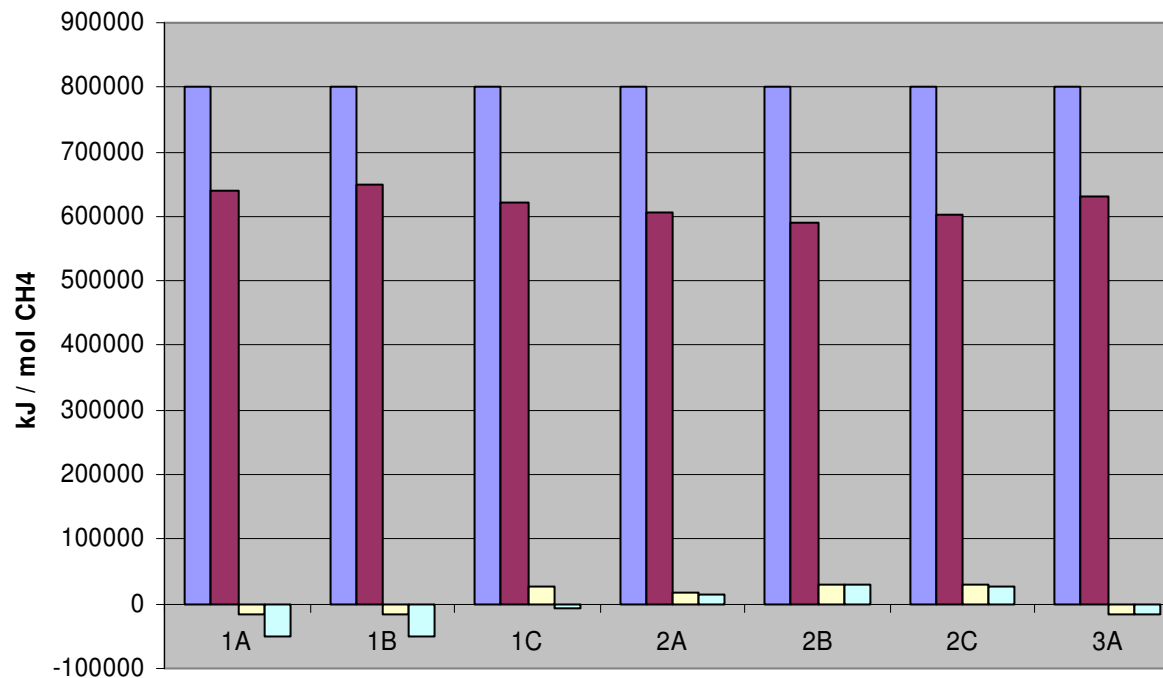


**Case 1A**  
Atmospheric CLR  
Partial oxidation



**Case 2B**  
Pressurized CLR 15 bar  
Autothermal Reforming  
Combined cycle with  
internal H<sub>2</sub> combustor

# HYDROGEN AND POWER



■ CH4 (LHV) 
 ■ H2 (LHV) 
 ■ Net Power 
 ■ Net Power (includes H2 compression to 20 bar)

**1A:** Atmospheric CLR, POX at 884 C

**1B:** Atmospheric CLR, ATR at 888 C

**1C:** Atmospheric CLR, ATR at 872C, steam cycle

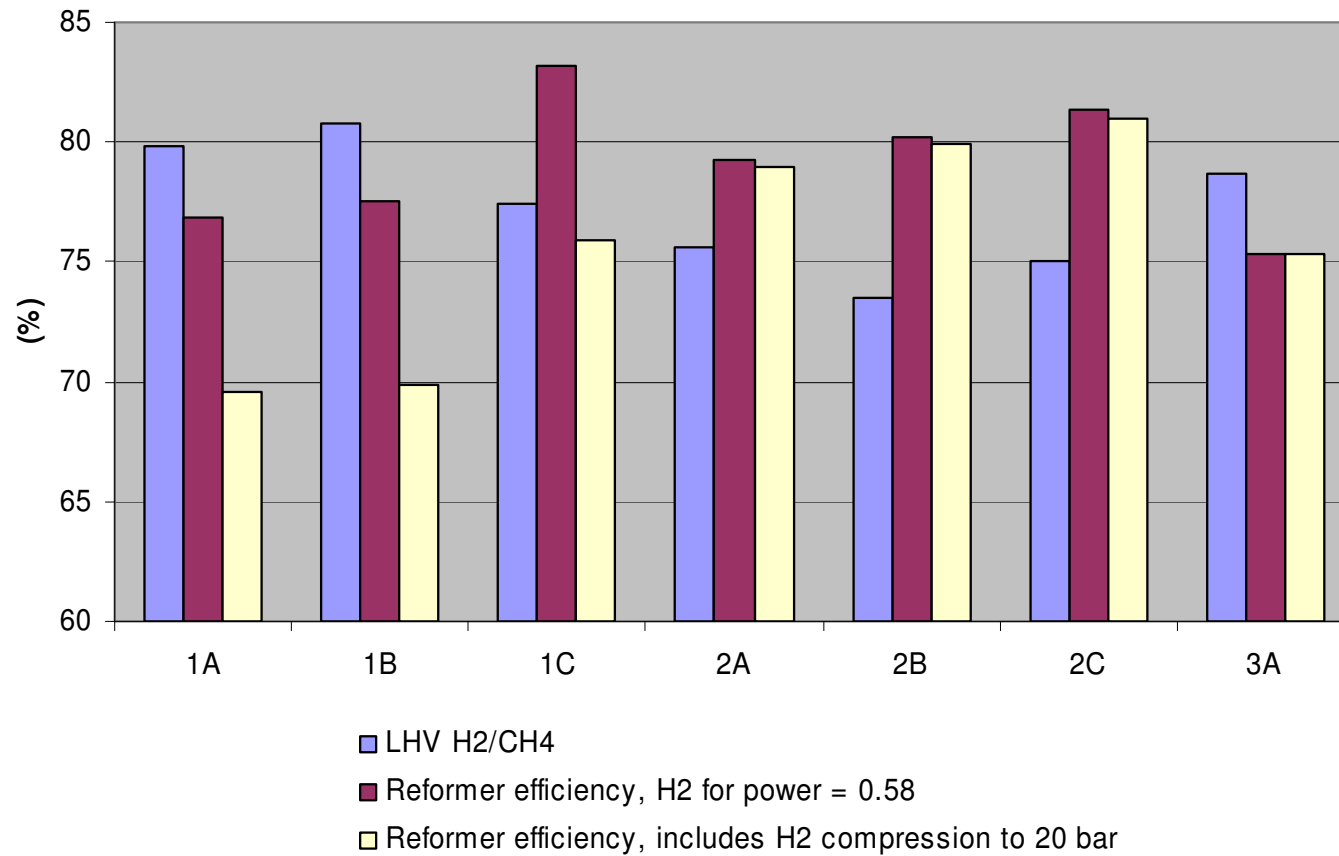
**2A:** CLR ATR at 15 bar, 1017C, combined cycle

**2B:** CLR ATR at 15 bar, 1000C, internal H2 combustor and combined cycle (0.11 H2 to internal combustion)

**2C:** CLR ATR at 15 bar, 1172C, combined cycle

**3A:** Steam reforming at 20 bar, 800C, with amine scrubbing (0.43 H2 and 0.14 CH4 to internal combustion)

# REFORMER EFFICIENCY



**1A:** Atmospheric CLR, POX at 884 C

**1B:** Atmospheric CLR, ATR at 888 C

**1C:** Atmospheric CLR, ATR at 872C, steam cycle

**2A:** CLR ATR at 15 bar, 1017C, combined cycle

**2B:** CLR ATR at 15 bar, 1000C, internal H2 combustor and combined cycle

**2C:** CLR ATR at 15 bar, 1172C, combined cycle

**3A:** Steam reforming at 20 bar, 800C, with amine scrubbing