

# **Pollutant formation and mitigation in combustion, Anders Lyngfelt**

**Overview**

**Sulphur**

**Nitrogen oxides**

**Incomplete combustion**

**CO<sub>2</sub> capture and storage in separate presentation**

# COMBUSTION

<u>component</u>	<u>emission</u>	<u>impact</u>	<u>measure</u>
CH <sub>x</sub>	CO <sub>2</sub> (not biofuel)	climate	<u>C</u> P F
-"-	volatile organic hydrocarbons etc	health, sec.air pollutants (SEP)*	<u>C</u> P
-"-	soot, low volatile polycyclic aromatic hydrocarbons (PAH)	health	<u>C</u> P
<hr/>			
N in air	NO <sub>x</sub> (thermal)	health, "SEP"	<u>C</u> P
N in fuel	NO <sub>x</sub> (fuel-) N <sub>2</sub> O	acid rain, eutrophication climate, str.ozon	<u>C</u> P

\*SEP, e.g. tropospheric ozone

measures:

C combustion, P post combustion, F change/clean fuel

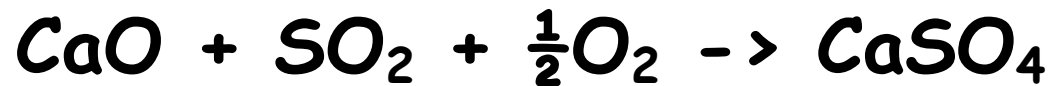
# COMBUSTION (CONTINUED)

<u>component</u>	<u>emission</u>	<u>impact</u>	<u>measure</u>
S	SO <sub>2</sub> , -> SO <sub>3</sub>	acid rain, environment, (health)	<u>C</u> P F
heavy metals	heavy metals	health, environm	P
Hg	Hg (=mercury)	health, environm	P
Cl (chlorine)	dioxins	health, environm	<u>C</u> P F
mineral ash	solid waste	place, leaching	(F)

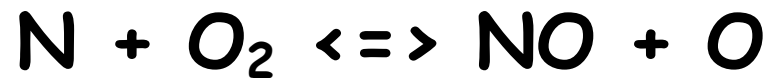
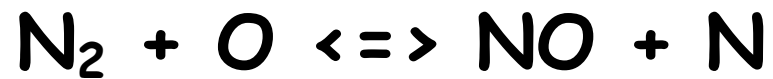
measures:

C combustion, P post combustion, F change/clean fuel

**sulphur capture in fluidized beds  
by addition of limestone**

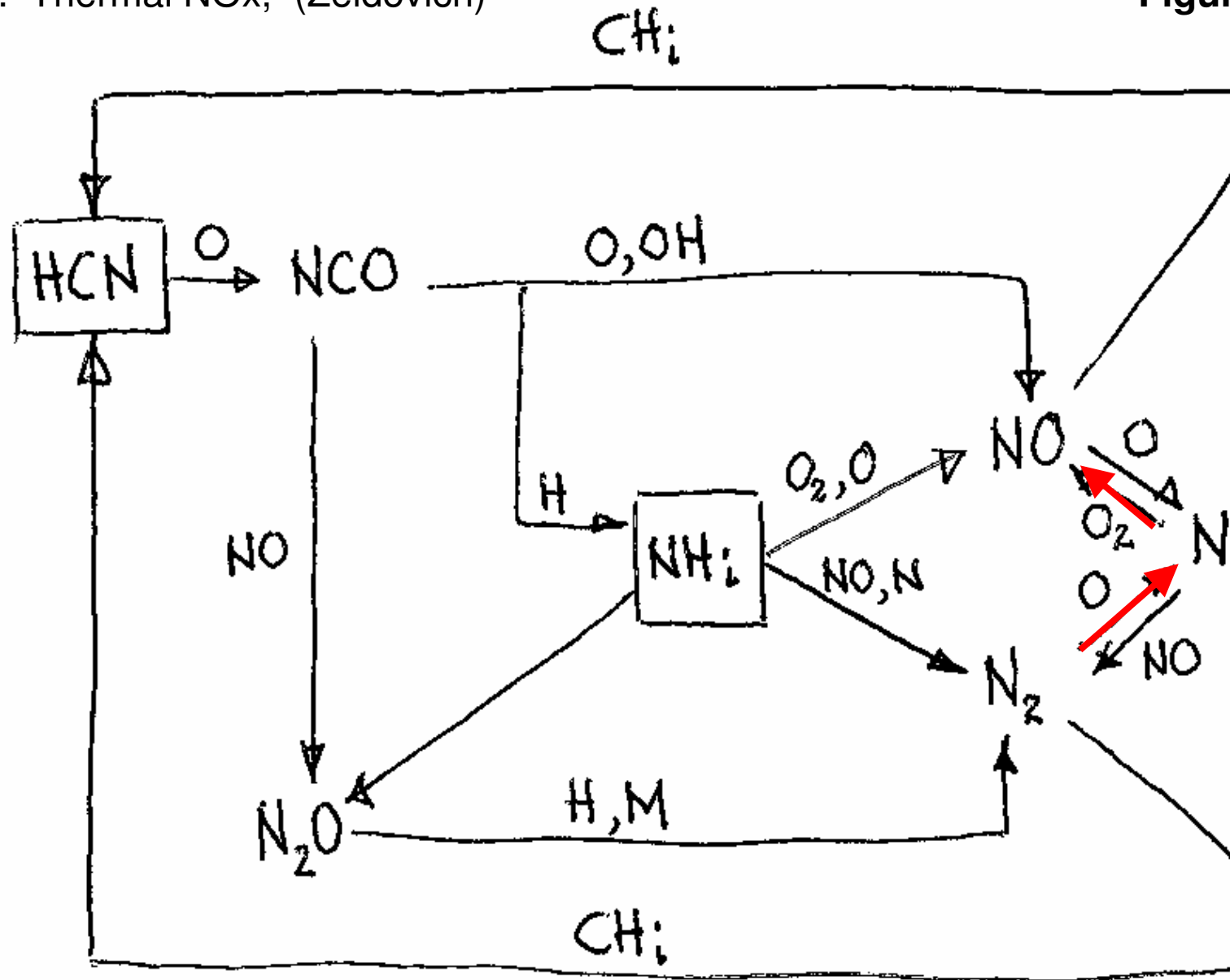


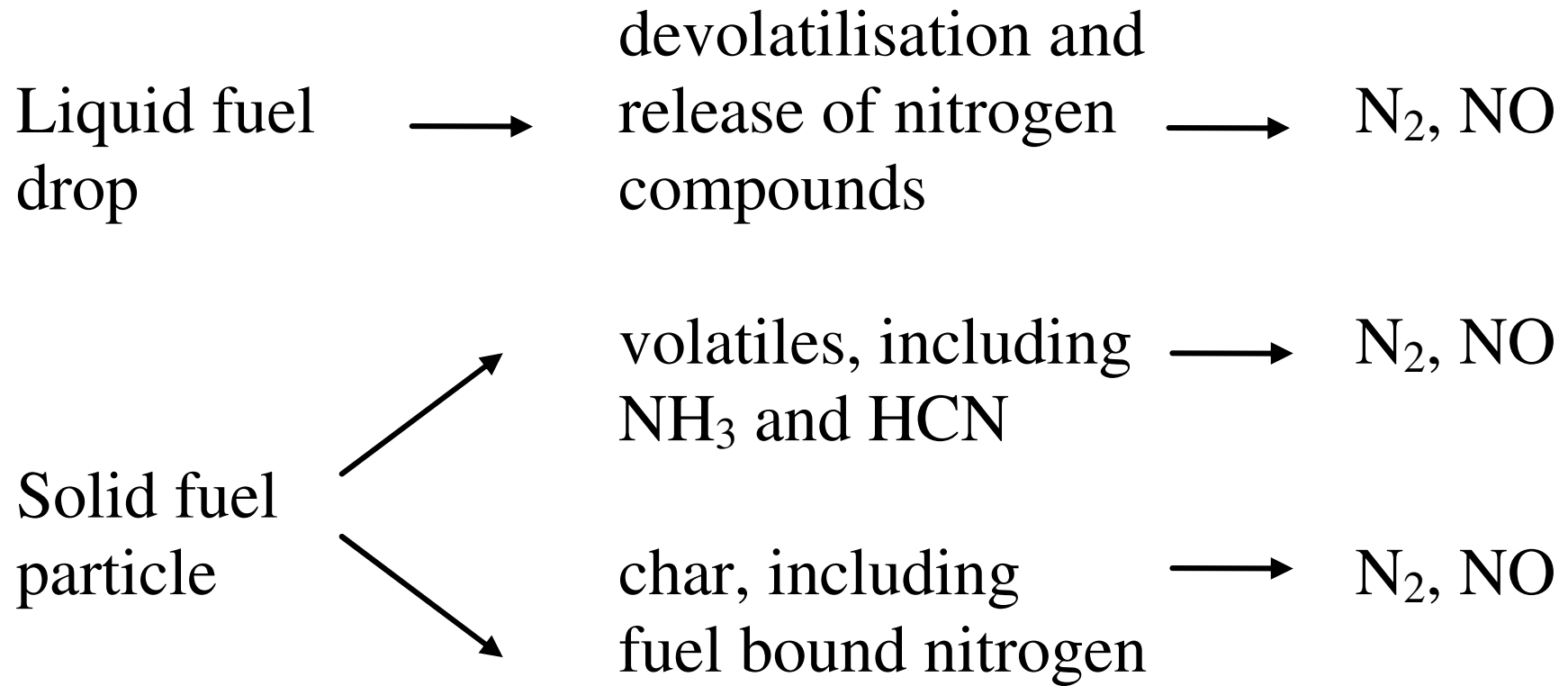
Thermal NO<sub>x</sub>, Zeldovich mechanism:



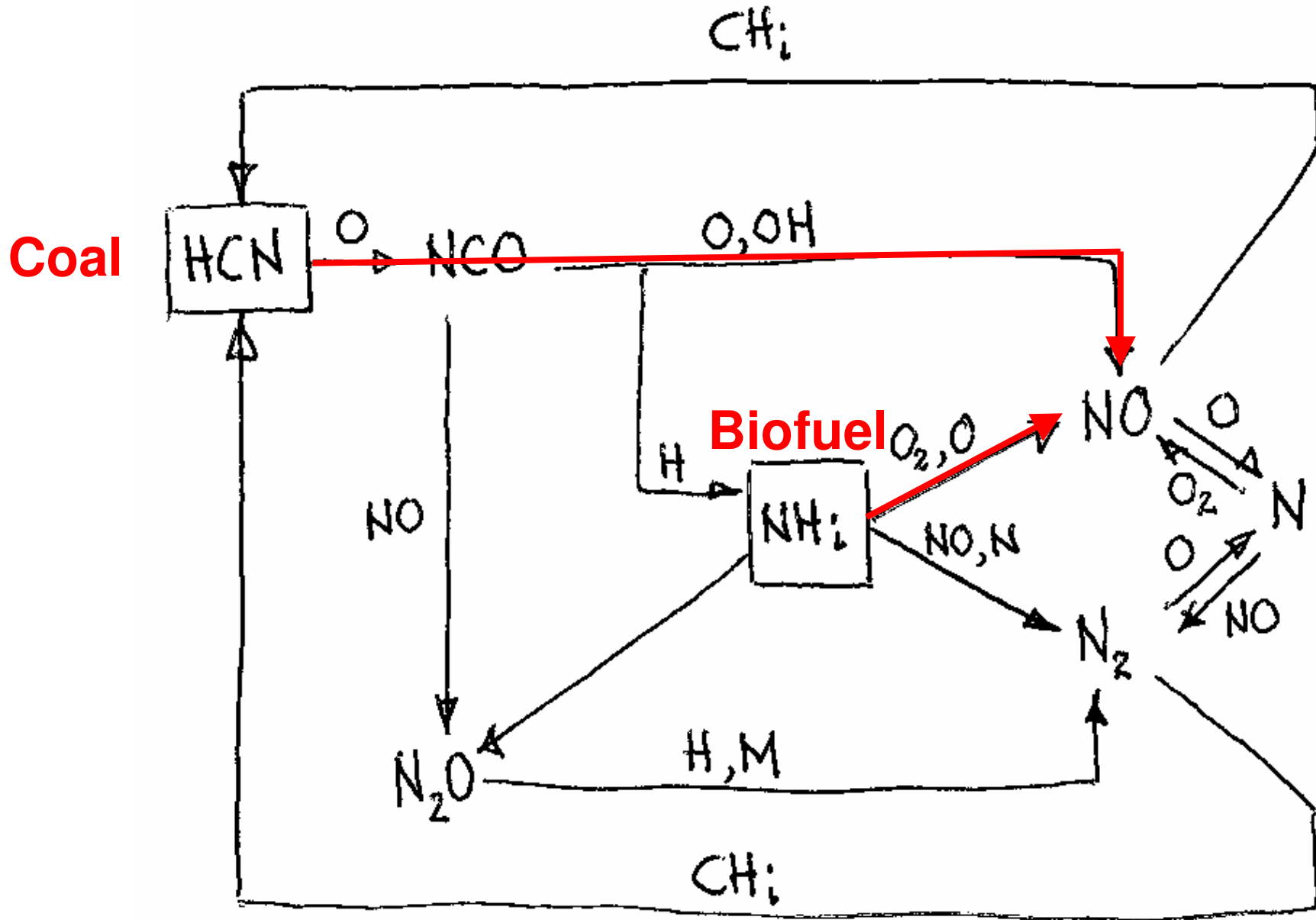
1. Thermal NOx, (Zeldovich)

Figure 10.2

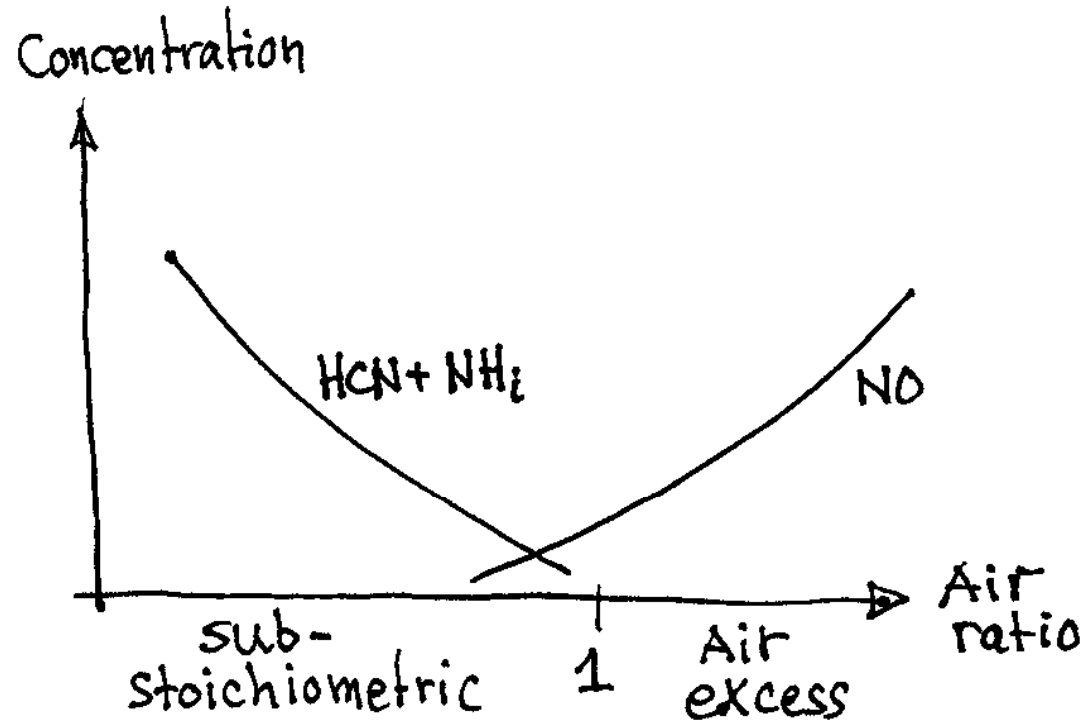




## 2. Fuel NO<sub>x</sub>

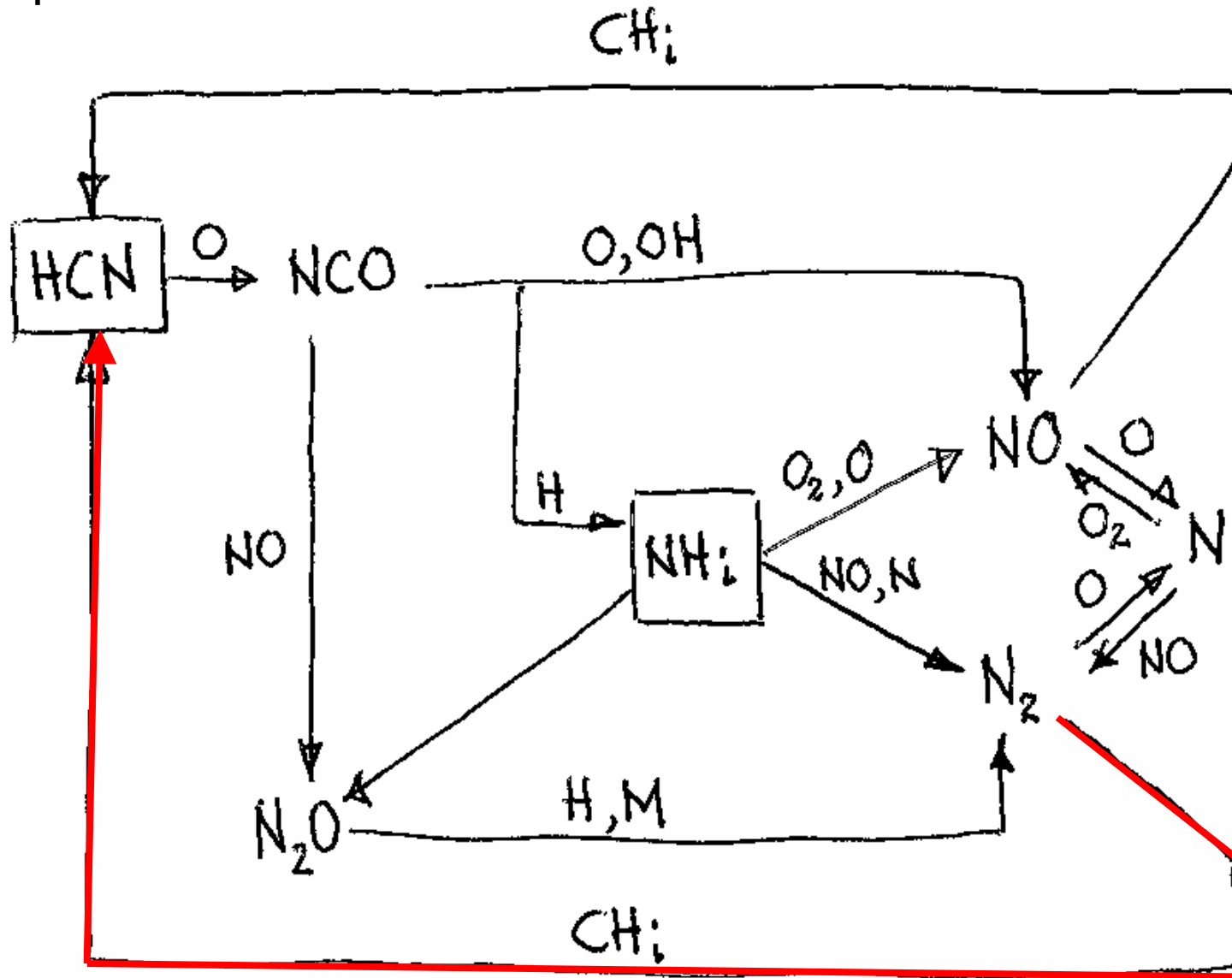




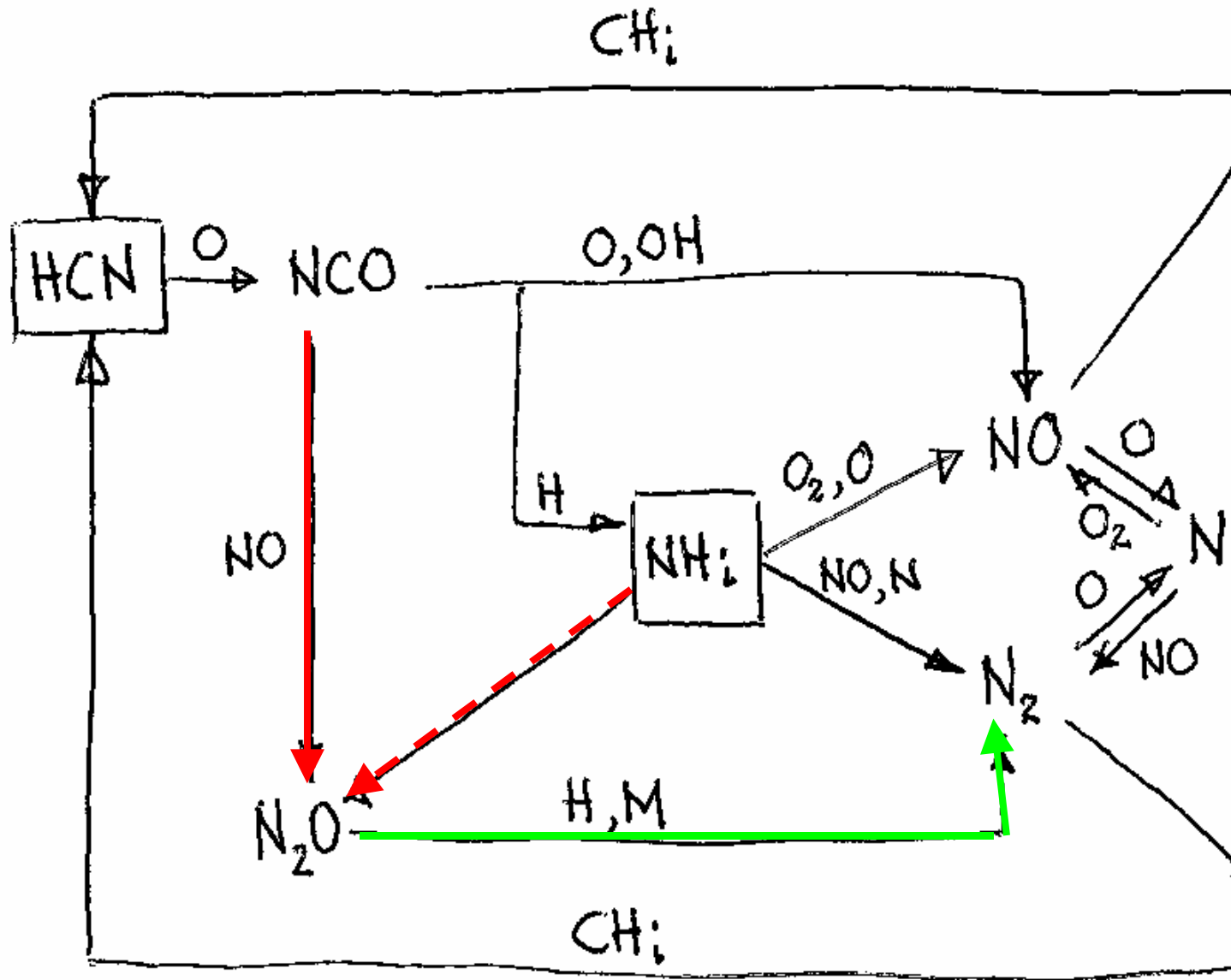


**Figure 10.3.**  
**Trade-off between unburned nitrogen compounds and nitrogen oxide**

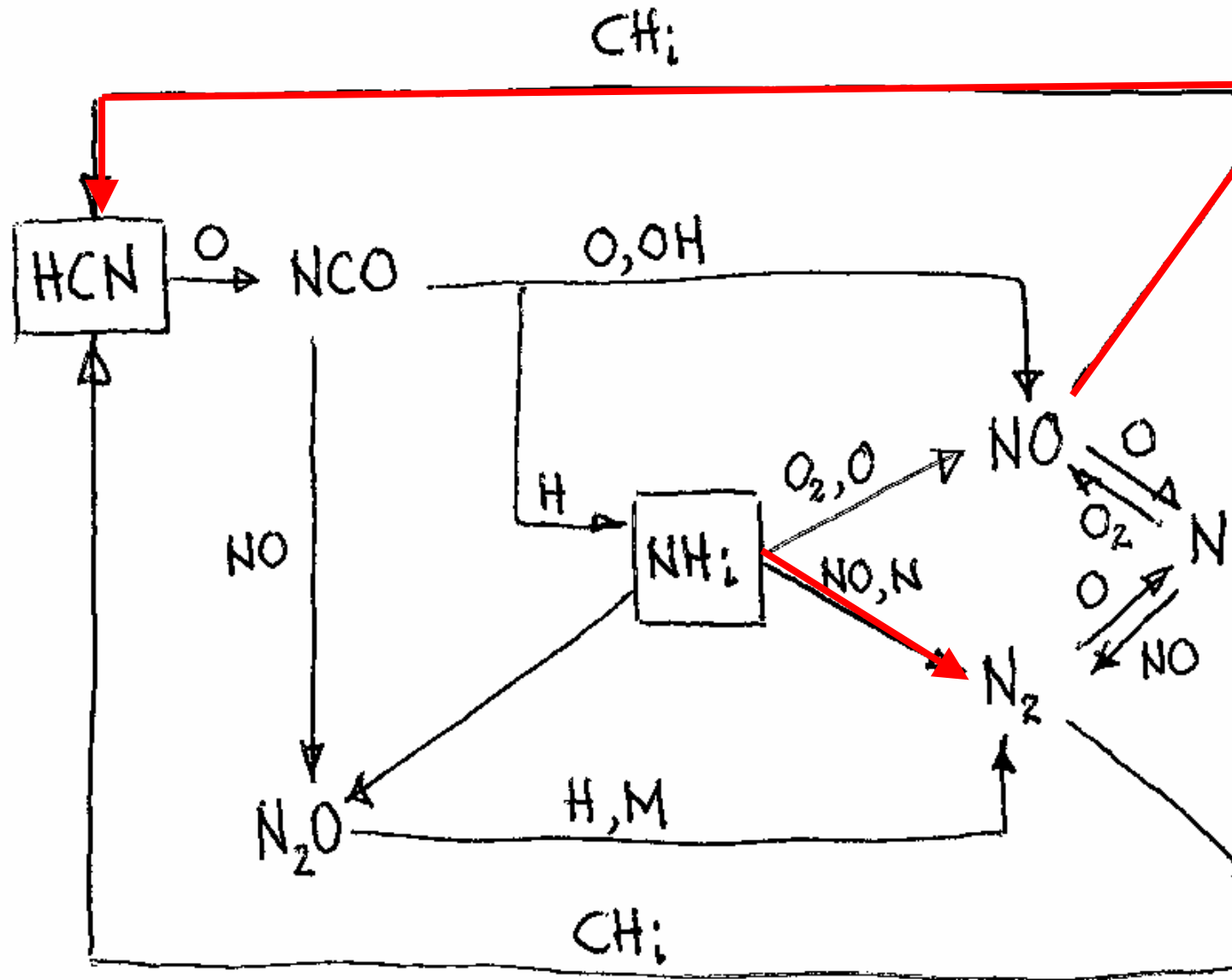
### 3. Prompt NOx

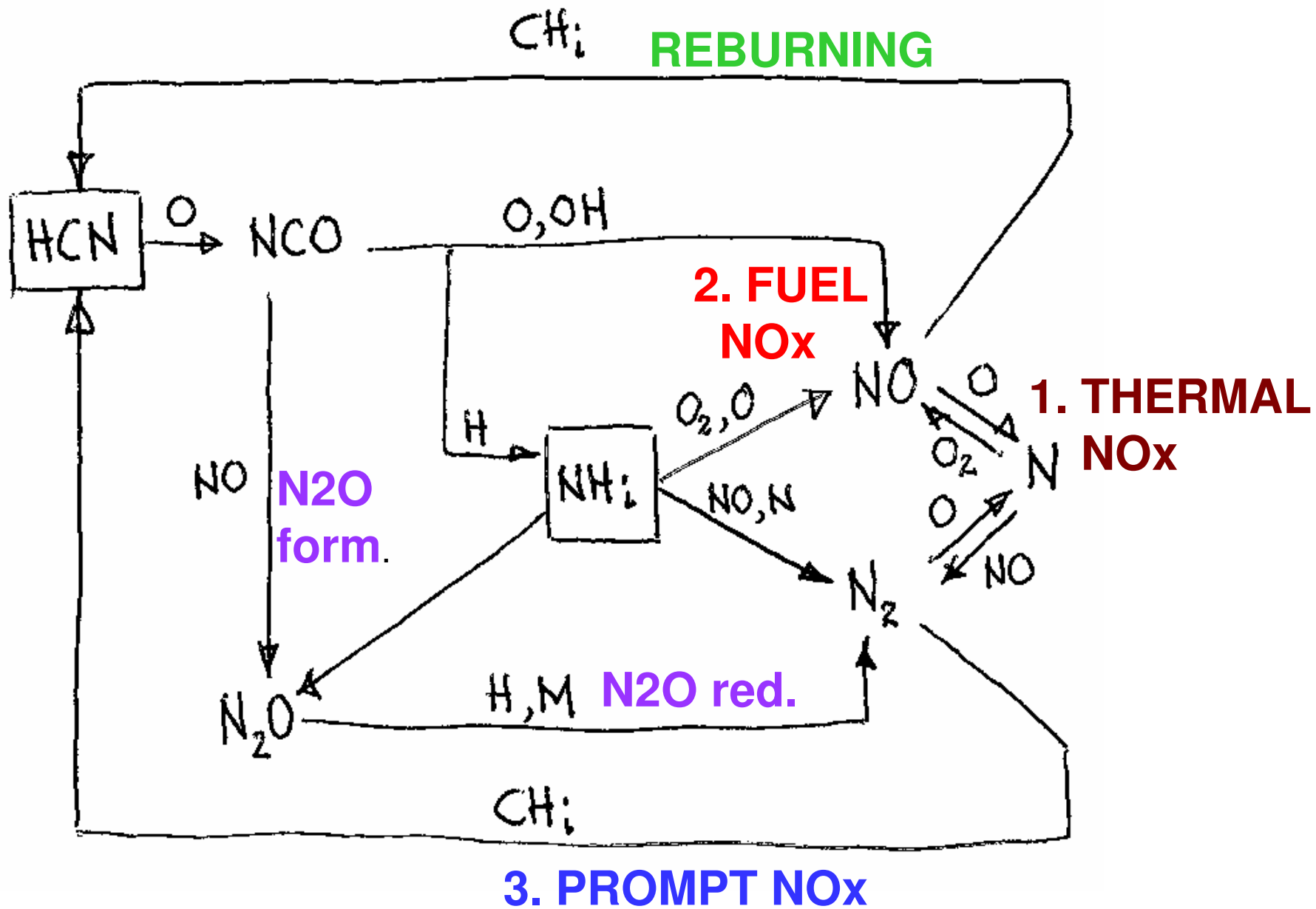


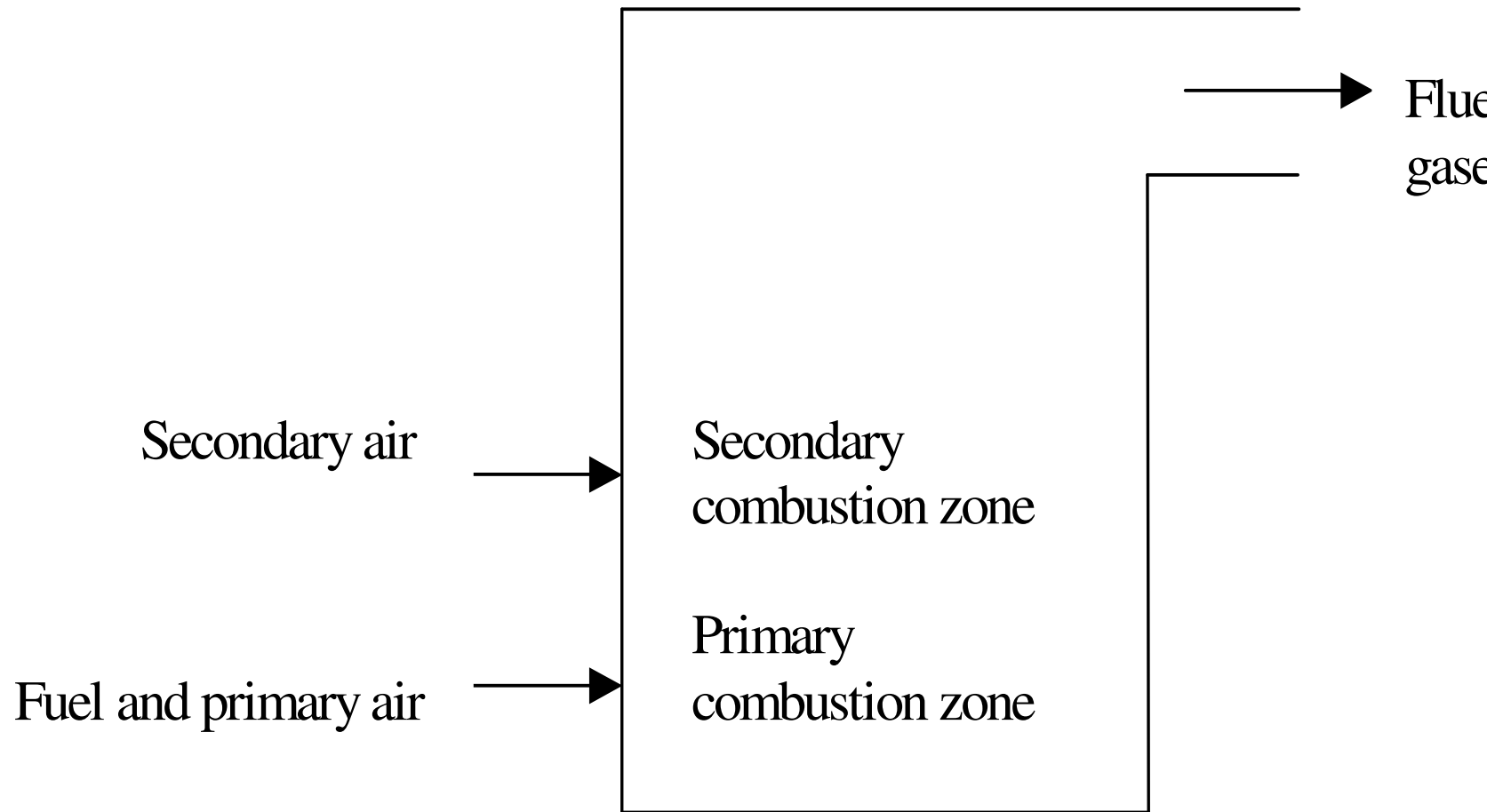
# N<sub>2</sub>O formation/reduction



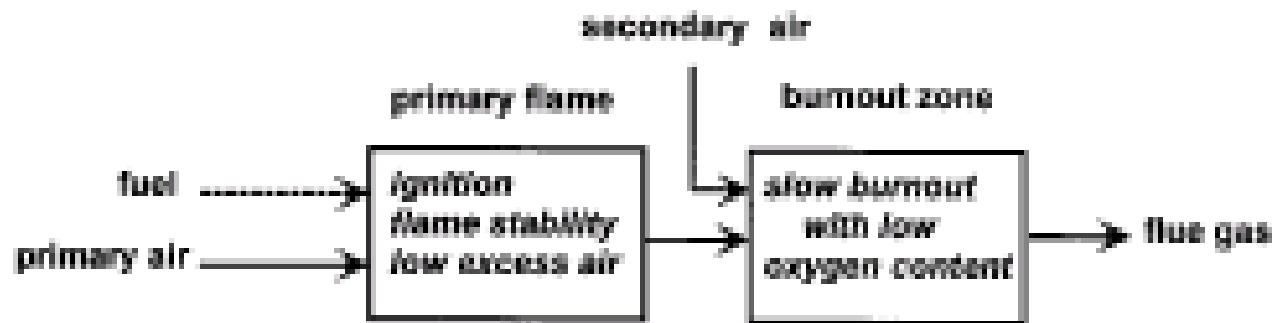
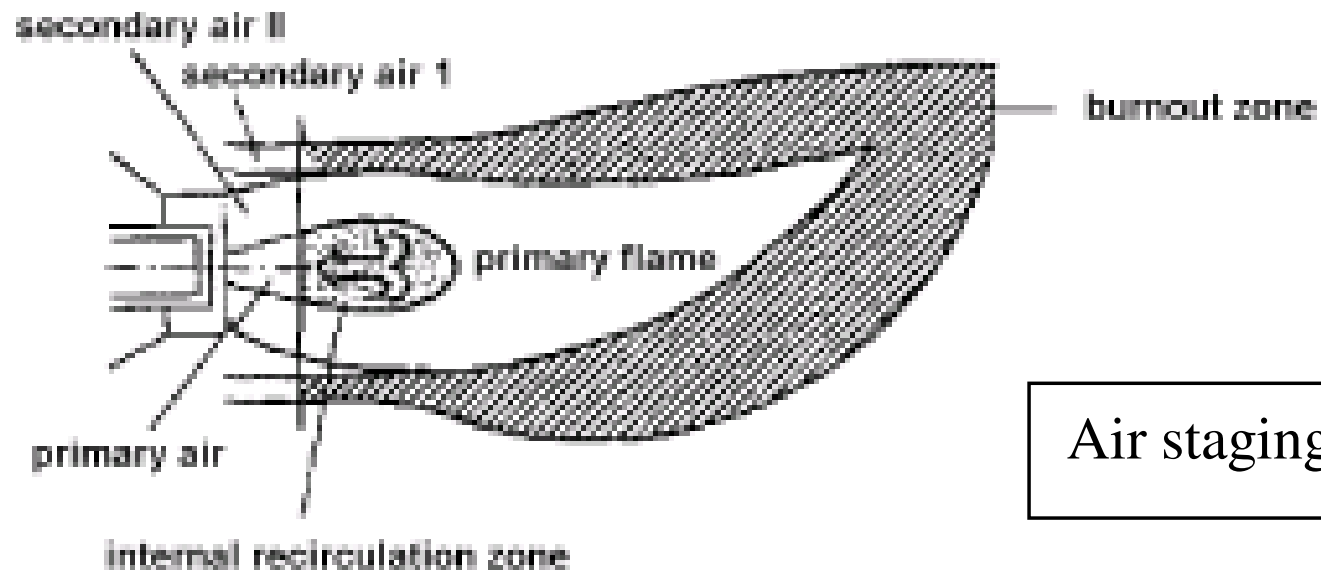
# Reburning

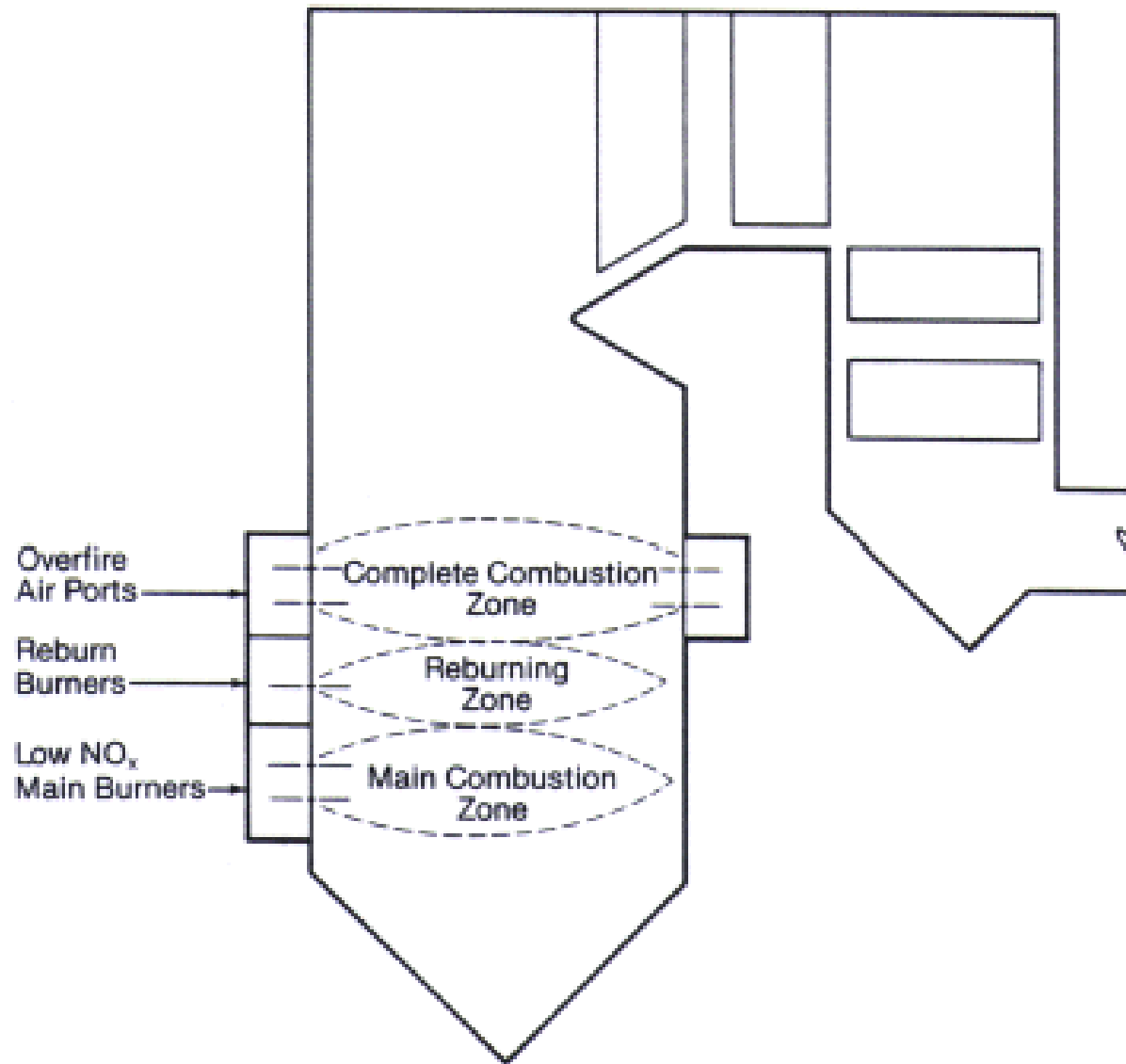






**Figure 10.4.**  
**Air staging in bed and suspension combustion**





**Figure 10.5. Reburning in a utility boiler**



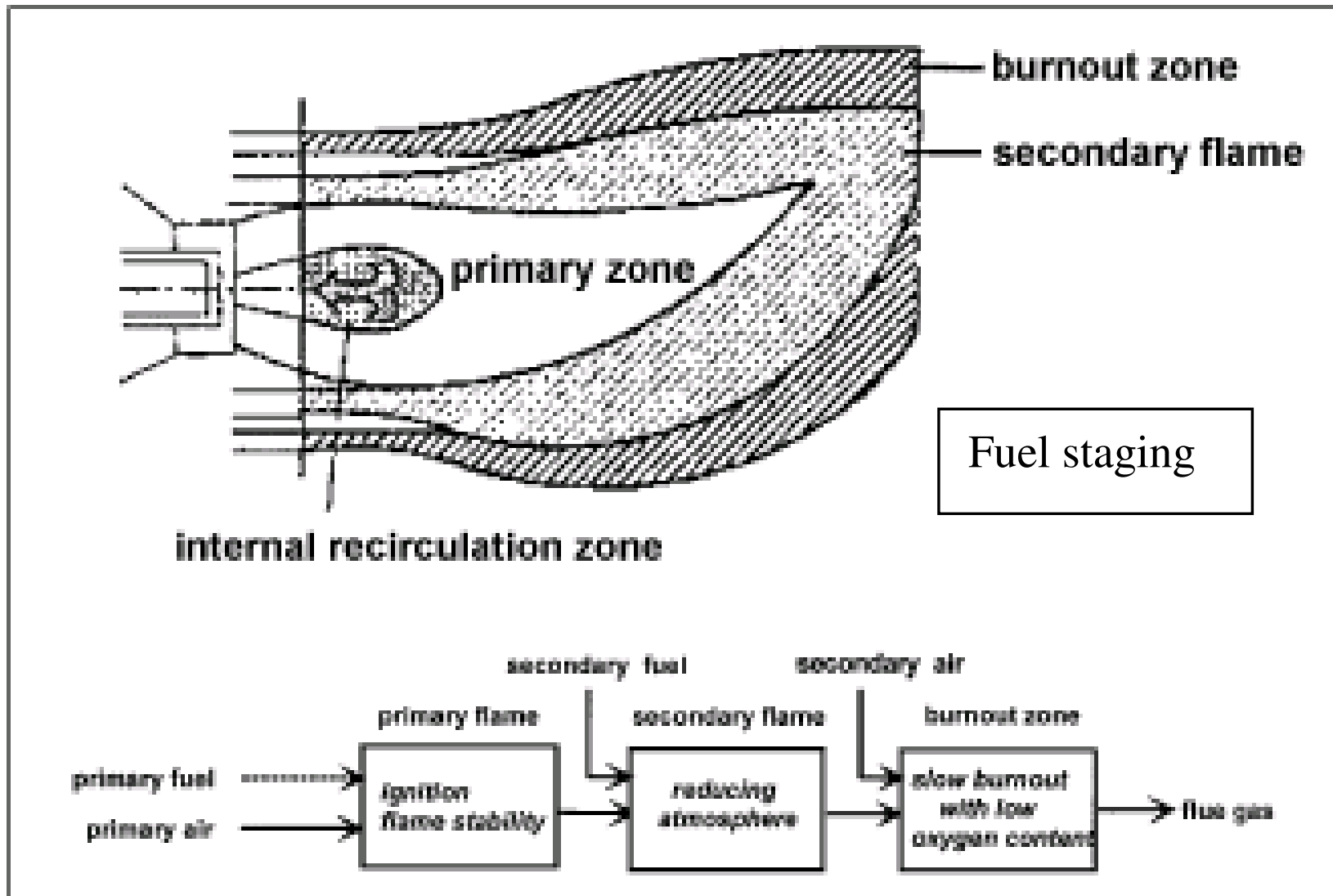
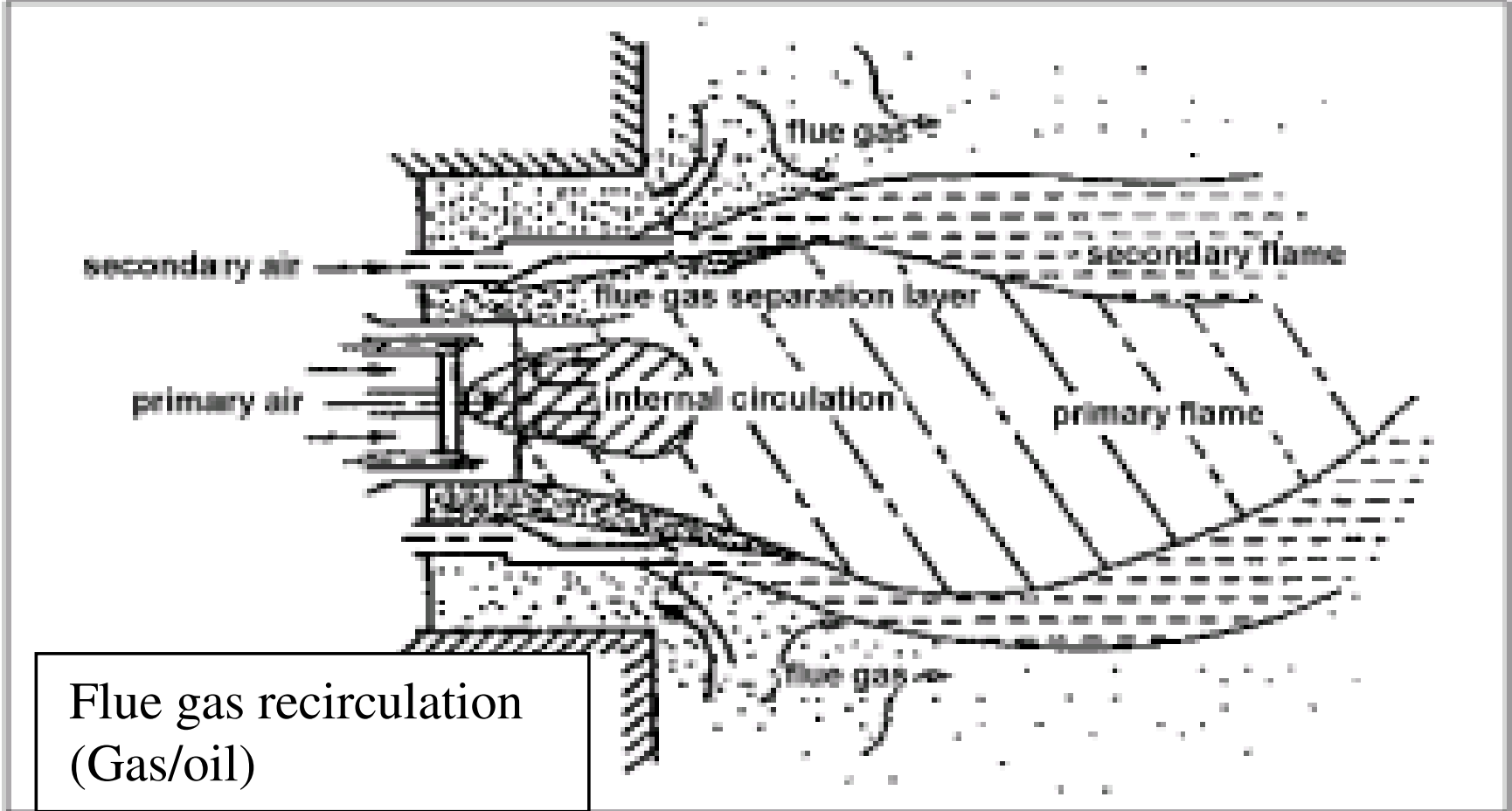


Figure 10.6.



Flue gas recirculation  
(Gas/oil)

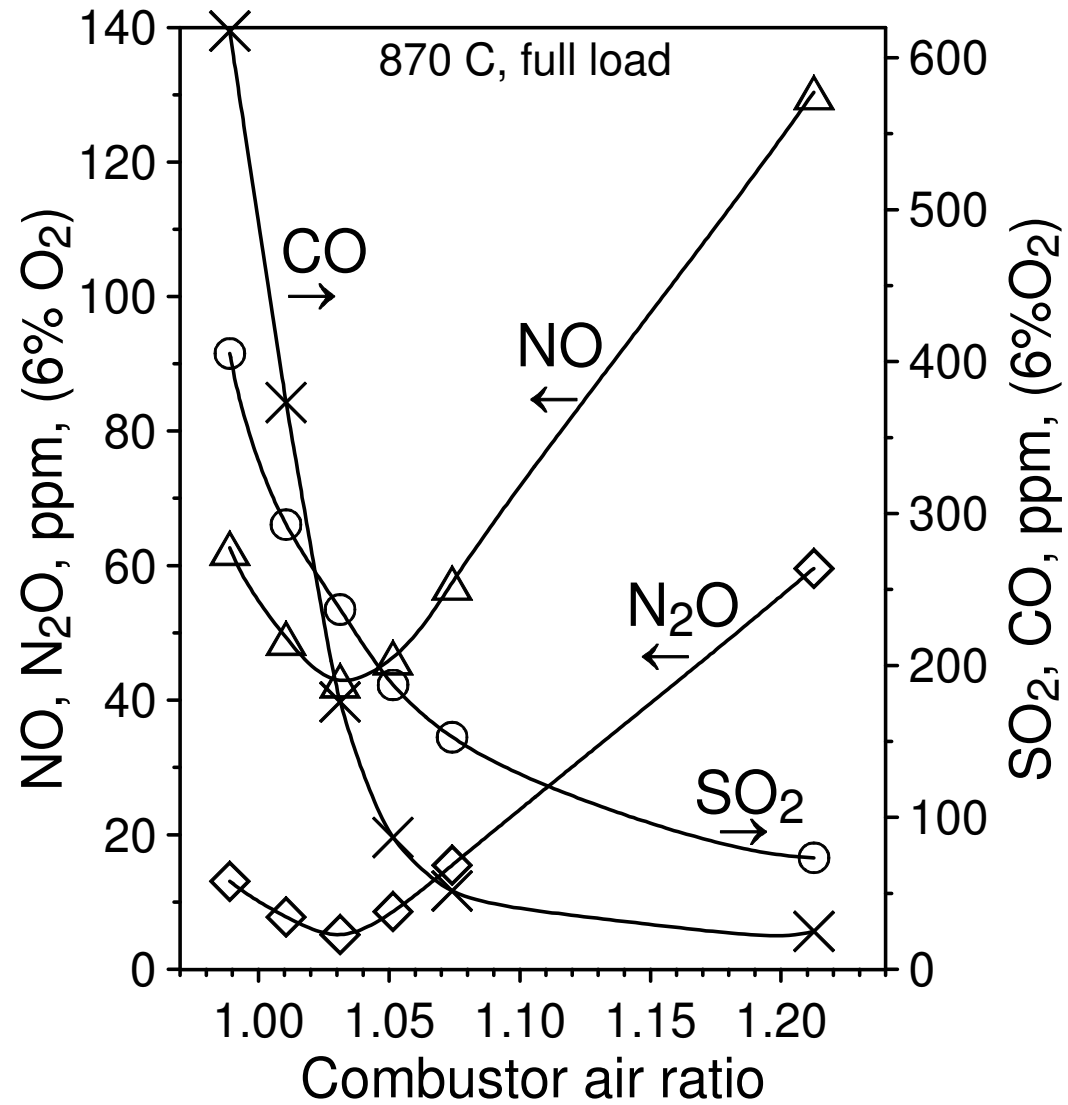
**Table 10.1. NO<sub>x</sub> reduction measures and their potential (van der Lans et al.)**

<b>Control Method</b>	<b>NO<sub>x</sub> reduction Potential*</b>	<b>Investigation and Baseline</b>
low excess air level	0-15%	(Guidelines for retrofit; study sponsored by EPRI) <sup>137</sup>
	10-15%	Lowering from 6 to 4% O <sub>2</sub> in several industrial installations with brown coal. Baselines from 200-350 ppm. <sup>138</sup>
over fire air	15-30%	(Review) <sup>139</sup>
	25%	Baseline 220 ppm in a 300 MW <sub>e</sub> boiler with brown coal. <sup>138</sup>
	20%	Baseline about 500 ppm in a tangentially fired furnace. <sup>140</sup>
	15%	Baseline about 300 ppm in a 600 MW <sub>th</sub> opposed-fired boiler. <sup>141</sup>
	15-50%	Typically 15% for wall-fired and 25% for tangentially fired. <sup>137</sup>
low NO <sub>x</sub> burners	23-40%	Two tangentially fired and two front wall-fired boilers. 40% reduction from baselines of 500-650 ppm, 23% reduction for 350 ppm

tangentially fired.<sup>137</sup>

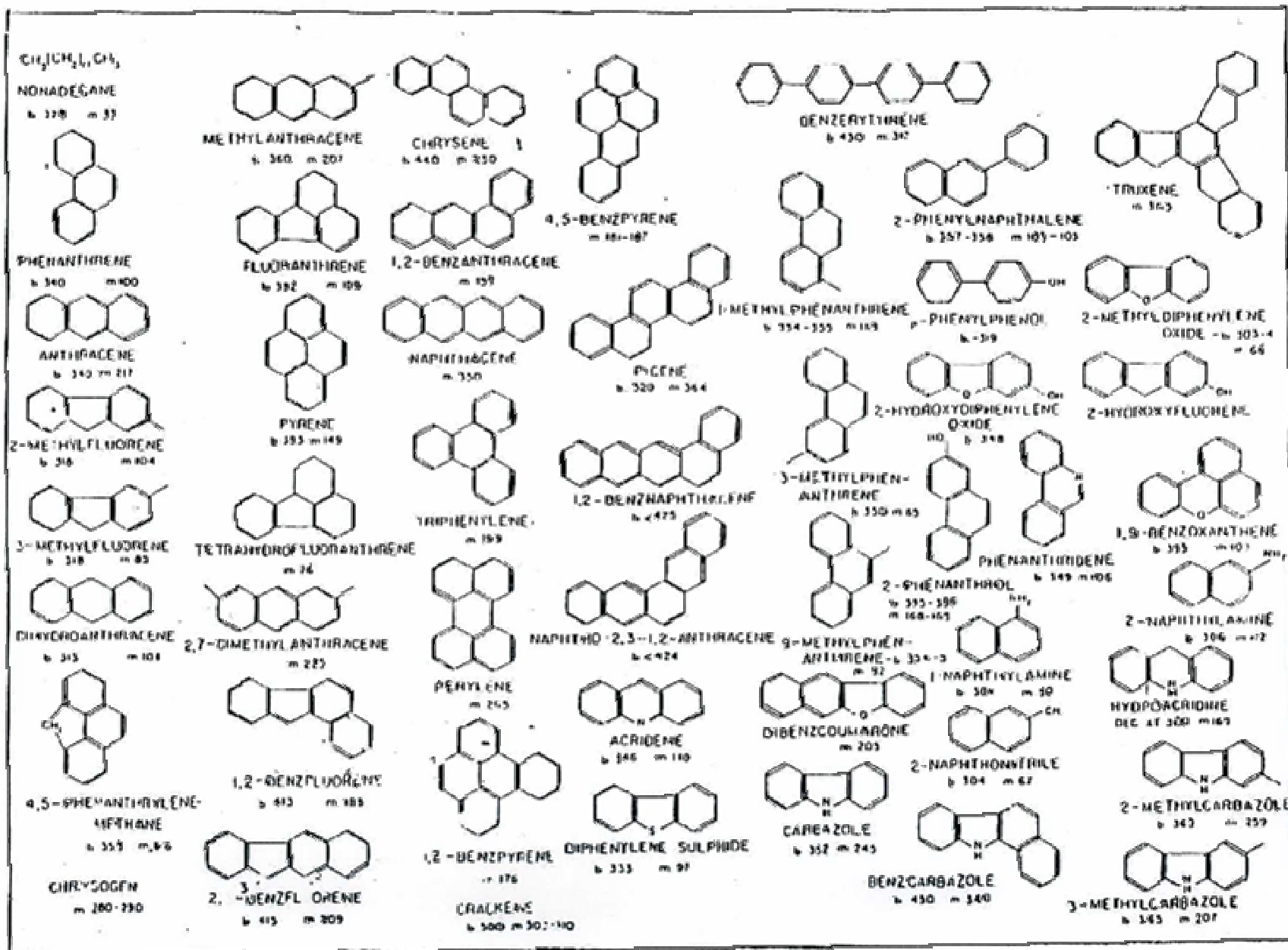
low NO <sub>x</sub> burners	23-40%	Two tangentially fired and two front wall-fired boilers. 40% reduction from baselines of 500-650 ppm, 23% reduction for 350 ppm as baseline. <sup>142</sup>
	50%	500 and 250 MW <sub>th</sub> wall-fired, baseline about 900 and 600 ppm respectively. <sup>143</sup>
	55%	600 MW <sub>e</sub> opposed-fired, baseline about 800 ppm. <sup>144</sup>
	40-70%	(Guidelines for retrofit; study sponsored by EPRI) <sup>137</sup>
flue gas recirculation	up to 30%	For wet bottom boilers; only few percent for dry bottom boilers (hard coal). <sup>139</sup>
	9-13%	150, 300 and 600 MW <sub>e</sub> boiler with brown coal. Baselines about 120 ppm, 10% recirculation. <sup>138</sup>
reburning	50%	300 MW <sub>e</sub> opposed-fired, baseline about 600 ppm. <sup>145</sup>
	60-70%	71 MW <sub>e</sub> tangentially fired (baseline about 550 ppm) and 158 MW <sub>e</sub> wall-fired (baseline about 400 ppm). <sup>146</sup>
SNCR	30-80%	(Review) <sup>139</sup>
SCR	60-90%	Most installations have been designed for a reduction around 60-70%, but over 90% can be reached at high initial NO concentration. <sup>139</sup>

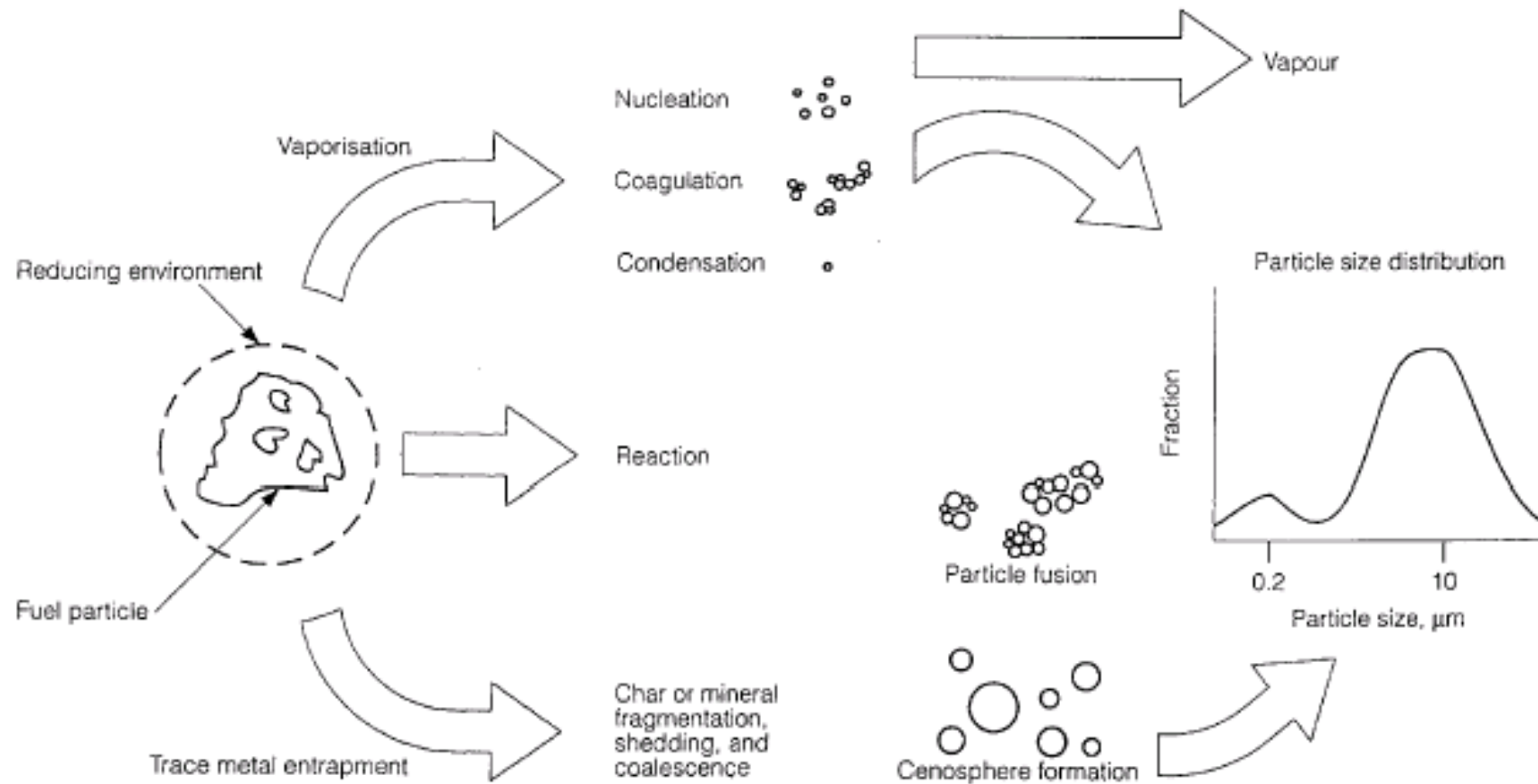
\* Compared to baseline value



**Figure 10.7.**  
**Emissions from a CFB boiler operated at 870° C and a total excess air ratio of 1.2. From Lyngfelt et al.**

Figur 35. Kok- och smältpunkter för olika PNA. Alla kokpunkter är >330 oc (ref 56).





**Figure 10.8.**  
**Distribution of trace elements during coal combustion. Davidson, 2000**